R&D of Photovoltaic Thermal (PVT) Systems: an Overview

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Article Info	ABSTRACT		
Article history:	Photovoltaic thermal (PVT), which is the popular technology for harvesting		
Received Dec 19, 2017 Revised Jan 18, 2018 Accepted Feb 3, 2018	solar energy, receive solar energy and convert it into electrical and therma energy simultaneously. In this review, design, heat transfer, energy modelling and performance analysis of PVT systems are presented. Fou types of PVT systems base on heat transfer medium; air-based PVT system water-based PVT system, the combination of water/air-based PVT system		
Keyword:	and nanofluid-based PVT system are presented. In addition, major finding on energy and exergy analysis of PVT systems are summarized.		
Energy analysis Exergy analysis Heat transfer			
Solar energy	Copyright © 2018 Institute of Advanced Engineering and Science. All rights reserved.		
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1. INTRODUCTION

The depletion of fossil fuels resources has revived the interest in renewable energy resource utilization [1]-[2]. As a result, various research and development (R&D) activities have been conducted to identify reliable and economically feasible alternative sources of clean energy. The choices include solar, wind, wave, and geothermal energies. Among these energy types, solar energy, which is widely used in heating and cooling applications, is the popular source [3]. Solar energy converts to electric energy using photovoltaic (PV) technology. The cons of this PV cell are declining in efficiency conversion when temperature raised and only responsive to a portion of the solar spectrum. The low efficiency and high cost of PV cell brings the idea of PVT system. It is the integration or hybrid of PV panel with solar thermal collector. The advantage of PVT enhances the electrical energy produce, removes waste heat from PV panel and minimized the usable space. Moreover, solar energy will convert to thermal energy as stored in air or water. PVT builds up from glass cover, solar cell, encapsulated materials and collector attached at the back. In terms of physical structure applied, the module could be classified as flat plate, concentrated and building integrated types. The absorber functions to absorb heat and simultaneously cool down the PV panel. The collected heat will be in the form of fluids or nanofluids.

Recently, energy and exergy analysis for PVT systems were studied base on experimental and theoretical study. A theoretical approach (mathematical model) to predict outlet and PV temperatures of finned PVT air collector system was studied [4]. The overall performance of the PVT system can be evaluated based on the thermodynamic, environmental and economic impacts analysis. Energy-exergy-economic-environmental analyses for different PVT array systems was studied [5]. In this review, thermodynamic analysis is focused involving Secondary Thermodynamic Law or known as exergy analysis. It has become an essential tool in the system design, analysis, and optimization of thermal systems [6-11].

2. TYPES OF PVT SYSTEMS

PVT is the popular technology of a solar energy technology. PVT system is a device designed to receive solar energy, convert it into electrical and thermal energy, which transfer the thermal energy to the fluid that flows into the collector. Fig. 1A shows a PVT consisting of a PV panel, insulation and frame. Accordingly, PVT consists of one or more cover (glass sheets) or a transparent material placed above an absorbing plate with air flowing around it. One way to enhance the collector's efficiency of PVT system is use heat transfer area through absorber with corrugated surfaces (Figs. 1B), finned absorber (Fig. 1C), and porous media (Fig. 1D). PVT system can be classified into four types base on heat transfer medium; airbased PVT system (Figs. 1A-D), water-based PVT system (Fig. 1E), the combination of water/air-based PVT system.



Figure 1. Various types of flat-plate PVT systems



Figure 2. Photograph of (a) honeycomb absorber installed at the back of PV panel, (b) PVT air collector with stainless porous media [12]



Figure 3. Combination of water/air-based PVT system; (a) schematic, (b) photograph [13]

3. ENERGY AND EXERGY ANALYSIS OF PVT SYSTEMS

The thermal efficiency of PVT system is a ratio of the useful thermal energy, Q_u to the overall incidence irradiations, I.

$$\eta_{th} = \frac{Q_u}{I}$$

The heat collected by the flat plate PVT collector can be measured by result of average mass flow rate, \dot{m} heat capacity of flowing medium, C_p and a temperature difference of the medium at the collector inlet, t_i and outlet, t_o [14-17].

$$Q_u = \dot{\mathrm{m}}C_p(t_o - t_i)$$

The electrical efficiency of PV, η_{pv} is a function of temperature given by

$$\eta_{pv} = \eta_r \big(1 - \beta (T_c - T_r) \big)$$

where η_r is the reference efficiency of the PV, β is the temperature coefficient ($\beta = 0.0045$ °C), T_c and T_r is cell temperature and the reference temperature [17].

Exergy is defined as the maximum amount of work that can be produced by a stream of matter, heat, or work as it reaches equilibrium with a reference environment. In the past few decades, exergy analysis has become an essential tool in thermal system design, analysis, and optimization [6-11]. If the effects of kinetic and potential energy changes are neglected, then the general exergy balance rate can be expressed in the following rate form:

$$\sum \mathbf{E} \mathbf{x}_{in} - \sum \mathbf{E} \mathbf{x}_o = \sum \mathbf{E} \mathbf{x}_d$$

Or

$$\sum \mathbf{E} \mathbf{X}_{in} - \sum \left(\mathbf{E} \mathbf{X}_{ih} + \mathbf{E} \mathbf{X}_{PV} \right) = \sum \mathbf{E} \mathbf{X}_{a}$$

where

$$\mathbf{E}\mathbf{x}_{d} = \mathbf{E}\mathbf{x}_{loss} = \mathbf{E}\mathbf{x}_{in} - \mathbf{E}\mathbf{x}_{o}$$

$$\mathbf{E}_{th} = mC(T_o - T_i) \left(1 - \frac{T_a + 273}{T_o + 273} \right)$$

 $E_{X_{PV}} = \eta A_c S$

$$\mathbf{E}_{in} = A_c N_c S \left[1 - \frac{4}{3} \left(\frac{T_a}{T_s} \right) + \frac{1}{3} \left(\frac{T_a}{T_s} \right)^4 \right]$$

The exergy and exergy efficiency of PVT system is expressed as $\mathbf{E} \mathbf{X}_{PVT} = \mathbf{E} \mathbf{X}_{th} + \mathbf{E} \mathbf{X}_{PV}$

$$\eta_{ex} = \frac{E_{x_o}}{E_{x_{in}}}$$

Exergy analysis may be proposed using the sustainability index (SI). It can be expresed as [18]

$$SI = \frac{1}{1 - \eta_{Ex}}$$

Another performance of exergy analysis is improvement potential (IP). It is useful to the efficient analysis of processes or systems. The IP of a process or system is calculated by [19, 20]:

$$IP = (1 - \eta_{Ex}) E x_{loss}.$$

where $\mathbf{E}_{\mathbf{X}_{PVT}}$ is the photovoltaic thermal exergy rate, $\mathbf{E}_{\mathbf{X}_{th}}$ is the thermal exergy rate, $\mathbf{E}_{\mathbf{X}_{in}}$ is the input exergy rate (radiation exergy rate), $\mathbf{E}_{\mathbf{X}_{o}}$ is the output exergy rate, S is the solar radiation, N_{c} is the collector's number, A_{c} is the collector area, T_{a} is the ambient temperature, and T_{s} is the sun temperature ($T_{s} = 5,777$ K).

Recently, Fudholi et al. [21] studied theoretical and experimental of PVT air collector with ∇ groove, as shown in Table 1. They reported that PVT energy efficiencies were 31.21-94.24%, and PVT exergy efficiencies of were 12.66-12.91%. The PV and thermal efficiency was 9.87-11.34% and 21.3-82.9% respectively. Several studies on the energy and exergy analysis of PVT systems were reported as shown in Table 2. Salem et al. [22] studied exergy and energy analysis of hybrid PVT system using aluminium cooling plate. They reported that PVT exergy efficiencies of were 11.1-13.5%, and PVT energy efficiencies were 59.3-92%. The PV and thermal efficiency was 17.7-38.4% and 31.6-57.9% respectively. Lari and Sahin [23] reported that PV energy efficiency was 13.2% for PVT nanofluid system. Khanjari et al. [24] reported that PV, thermal and PVT energy efficiencies was 10-13.7%, 55% and 90% respectively, and PVT exergy efficiency was 15%. Tripathi et al. [25] studied exergoeconomic and enviroeconomic analysis base on energy and exergy for PVT concentrating collector. They reported that thermal and PVT energy efficiencies were 40-50% and 45-63%, respectively. Singh et al. [26] studied energy and exergy for active solar still integrated with two hybrid PVT collectors. They reported that thermal and PVT energy efficiencies was 69.06% and 75%, respectively. Energy and exergy analyses for PVT air collectors were studied [27, 28]. Hazami et al. [27] and Gholampour and Ameri [28] reported that PVT exergy efficiency was 14.8% and 8.66%, respectively. Exergoeconomic and environmental analyses for PVT mixed mode greenhouse solar dryer was studied [29]. They reported that PVT energy efficiency was 68.5%. Exergoeconomicenviroeconomic--environmental-exergy-energy analyses were studied for active solar distillation system [32] in 2015.



Figure 4. Photograph of (a) PVT collector with ∇ -groove, (b) PVT collector under solar simulator

Tables 1. Schematic diagram of heat	transfer characteristics and	a mathematical model of PV	T air collector
	with ∇ -groove		

The steady-state energy balance equations for PVT air collector with $\nabla_{-grove as below:}$ For PV, $r\alpha G = U_i (T_p - T_a) + h_i (T_p - T_f) + h_{qp} G + Q_a$ The steady-state energy balance equations for PVT air collector with $\nabla_{-grove as below:}$ For PV, $r\alpha G = U_i (T_p - T_a) + h_i (T_p - T_f) + h_{qp} G + Q_a$ For air flow channel, $mC(T_a - T_f) = h_i (T_p - T_f) + h_2 (T_b - T_f) + Q_a$ For back plate, $h_{ppb} (T_p - T_b) = h_2 (T_b - T_f) + U_b (T_b - T_a)$ Where, $Q_a = NA_a h_i \eta_a (T_p - T_f)$ $\eta_a = \frac{\tanh MH}{MH}$ $M = \left(\frac{2h_i l}{k_a A_{ca}}\right)^N$ $M_b = \frac{k}{l_i}$ $U_i : collector back loss coefficient (W/m^{1*}C)$ u: anbiarit temperature (C) $T_i : anbiarit temperature (C)$ $T_i : bert of a (JkgoC)$ $T_i : bert of a (Jkgo$		e
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For PV, $T_{p} \longrightarrow T_{h_{m}} \longrightarrow T_{r_{h_{m}}} \longrightarrow$	STATE AND STATE	
$\begin{aligned} & \tau \alpha G = U_{i} (T_{p} - T_{a}) + h_{i} (T_{p} - T_{b}) + h_{p,b} (T_{p} - T_{b}) + \eta_{p} G + Q_{a} \\ & \tau \alpha G = U_{i} (T_{p} - T_{a}) + h_{i} (T_{p} - T_{f}) + h_{p,b} (T_{p} - T_{b}) + \eta_{p} G + Q_{a} \\ & \tau \alpha G = U_{i} (T_{p} - T_{i}) + h_{i} (T_{p} - T_{f}) + \eta_{p} G + Q_{a} \\ & T_{b} = \int_{0}^{1} \int_$	$\alpha \tau G = U_t$	For PV,
$T_{p} \underbrace{V_{p}}_{T_{b}} \underbrace{V_{p}}_{T_{b}$	h _w	$\tau \alpha G = U_{t}(T_{p} - T_{a}) + h_{t}(T_{p} - T_{f}) + h_{rpb}(T_{p} - T_{b}) + \eta_{p}G + Q_{n}$
For air flow channel, $mC(T_{a} - T_{i}) = h_{i}(T_{p} - T_{f}) + h_{2}(T_{b} - T_{f}) + Q_{a}$ For back plate, $h_{rpb}(T_{p} - T_{b}) = h_{2}(T_{b} - T_{f}) + U_{b}(T_{b} - T_{a})$ Where, $h_{rpb}(T_{p} - T_{b}) = h_{2}(T_{b} - T_{f}) + U_{b}(T_{b} - T_{a})$ Where, $Q_{a} = NA_{a}h_{i}\eta_{a}(T_{p} - T_{f})$ $\eta_{a} = \frac{\tanh MH}{MH}$ $M = \left(\frac{2h_{i}l}{k_{a}A_{ca}}\right)^{N}$ $U_{b} = \frac{k_{i}}{l_{i}}$ $U_{b} = \frac{k_{i}}{l_{i}}$ $U_{b} = \frac{k_{i}}{l_{i}}$ $U_{b} = \frac{m_{i}}{k_{i}}$ $H_{rpb}(T_{p} - T_{b}) = h_{2}(T_{b} - T_{f}) + U_{b}(T_{b} - T_{a})$ Where, $Q_{a} = NA_{a}h_{i}\eta_{a}(T_{p} - T_{f})$ $M_{b} = \frac{k_{i}}{MH}$ $M = \left(\frac{2h_{i}l}{k_{a}A_{ca}}\right)^{N}$ $U_{b} = \frac{k_{i}}{l_{i}}$ $U_{b} = \frac{k_{i}}{l_{i}}$ $H_{rpb}(T_{p} - T_{b}) = h_{2}(T_{p} - T_{b})$ $H_{rpb}(T_{p} - T_{b}) = h_{2}(T_{p} - T_{b})$ $H_{rpb}(T_{p} - T_{b}) = h_{2}(T_{p} - T_{b}) = h_{2}(T_{p} - T_{b})$	T _a	
$ \begin{array}{l} mC(T_{a}-T_{i})=h_{1}(T_{p}-T_{f})+h_{2}(T_{b}-T_{f})+Q_{a} \\ mC(T_{a}-T_{i})=h_{1}(T_{p}-T_{f})+h_{2}(T_{b}-T_{f})+Q_{a} \\ \\ \text{For back plate,} \\ h_{rpb}(T_{p}-T_{b})=h_{2}(T_{b}-T_{f})+U_{b}(T_{b}-T_{a}) \\ \\ \text{Where,} \\ Q_{a}=NA_{a}h_{i}\eta_{a}(T_{p}-T_{f}) \\ \\ Where, \\ Q_{a}=NA_{a}h_{i}\eta_{a}(T_{p}-T_{f}) \\ \\ \\ Where, \\ Q_{a}=NA_{a}h_{i}\eta_{a}(T_{p}-T_{f}) \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\$	$\Delta A A A A$	For air flow channel,
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$\begin{split} & \bigvee_{U_b} & h_{ipb}(T_p - T_b) = h_2(T_b - T_f) + U_b(T_b - T_a) \\ & & \text{Where,} \\ \text{h. heat transfer coefficient (W/m^{10}\text{C})} \\ & & \text{U}_b \text{ collector back loss coefficient (W/m^{10}\text{C})} \\ & & \text{U}_b \text{ collector back loss coefficient (W/m^{10}\text{C})} \\ & & \text{U}_b \text{ collector back loss coefficient (W/m^{10}\text{C})} \\ & & \text{utransistion coefficient} \\ & & \text{transistion coefficient} \\ &$		For back plate,
$\begin{split} & \bigvee_{U_b} & & \text{Where,} \\ Q_a &= NA_a h_c \eta_a \left(T_p - T_f\right) \\ & & Q_a &= NA_a h_c \eta_a \left(T_p - T_f\right) \\ & & Q_a &= NA_a h_c \eta_a \left(T_p - T_f\right) \\ & & Q_a &= NA_a h_c \eta_a \left(T_p - T_f\right) \\ & & Q_a &= NA_a h_c \eta_a \left(T_p - T_f\right) \\ & & \eta_a &= \frac{\tanh MH}{MH} \\ & & M = \left(\frac{2h_c I}{k_a A_{ca}}\right)^{N_c} \\ & & Q_a &= NA_a h_c \eta_a \left(T_p - T_f\right) \\ & & M = \left(\frac{2h_c I}{k_a A_{ca}}\right)^{N_c} \\ & & Q_a &= NA_a h_c \eta_a \left(T_p - T_f\right) \\ & & M = \left(\frac{2h_c I}{k_a A_{ca}}\right)^{N_c} \\ & & Q_a &= NA_a h_c \eta_a \left(T_p - T_f\right) \\ & & M = \left(\frac{2h_c I}{k_a A_{ca}}\right)^{N_c} \\ & & M = \left(\frac{2h_c I}{k_a A_{ca}}\right)^{N_c} \\ & & U_b &= \frac{k_c}{l_c} \\ & & U_f &= \left(\frac{1}{h_w + h_{pw}}\right)^{-1} \\ & & U_f &= \left(\frac{1}{h_w + h_{pw}}\right)^{-1} \\ & & H_{pw} &= \frac{\sigma \left(T_p + T_b \right) \left(T_p^2 + T_b^2\right)}{\left(\frac{1}{k_p} + \frac{1}{k_p} - 1\right)} \\ & & h_{pw} &= \mathcal{E}_p \sigma \left(T_p^2 + T_{aby}^2\right) \left(T_p - T_{aby}\right) \\ & & T_{aby} &= 0.0522 T_a^{1.5} \\ & & h_1 &= h_2 &= h_c \\ \end{array}$		$h_{rpb}(T_p - T_b) = h_2(T_b - T_f) + U_b(T_b - T_a)$
$\begin{split} U_b & Q_a = NA_a h_c \eta_a (T_p - T_f) \\ & \\ & \\ & \\ & \\ & \\ & \\ & \\ & \\ & \\ $	\checkmark	Where,
$ \begin{array}{ll} & \text{Where,} \\ \text{h: heat transfer coefficient (W/m^{2n} \mathbb{C})} \\ \text{h: collector back loss coefficient (W/m^{2n} \mathbb{C})} \\ \text{U}_{i: collector back loss coefficient (W/m^{2n} \mathbb{C})} \\ \text{U}_{i: collector back loss coefficient} \\ \text{S: missistic coefficient} \\ \text{S: collector halphate temperature (C)} \\ \text{T_{i: back lost bast of an (J/kg o \mathbb{C})} \\ \text{m: mass flow rate (kg/s)} \\ \text{H: collector height(m)} \\ \text{K: thermal conductivity (W/m^{\circ} \mathbb{C})} \\ \text{A: area (m^{2})} \\ \end{array} $ $ \begin{array}{l} & h_{qw} = \mathcal{E}_{p} \sigma \left(T_{p}^{-} + T_{aky}^{-}\right) \left(T_{p} - T_{aky}\right) \\ & h_{qw} = \mathcal{E}_{p} \sigma \left(T_{p}^{-} + T_{aky}^{-}\right) \left(T_{p} - T_{aky}\right) \\ & T_{aky} = 0.0522 T_{a}^{1.5} \\ & h_{i} = h_{c} = h_{c} \end{array} $	U_b	$Q_n = NA_n h_e \eta_n (T_p - T_f)$
h: heat transfer coefficient (W/m ^{4/2} C) U:: collector back loss coefficient (W/m ^{4/2} C) U:: collector top loss coefficient (W/m ^{4/2} C) a: absorption coefficient t: transmission coefficient t: collector back plate temperature (°C) T_i: back plate temperature (°C) T_i: sky temperature (°C) C: Specific heat of air (J/kg oC) m: mass flow rate (kg/s) H: collector height (m) k: thermal conductivity (W/m °C) A: area (m ²) $h_{que} = c_p \sigma (T_p^2 + T_{dy}^2) (T_p - T_{dy})$ $H_{que} = h_c$	Where,	tanh MH
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U: collector top loss coefficient (W/m ⁻⁺ C) a: absorption coefficient f: transmission coefficient f: transmission coefficient f: transmission coefficient f: collactor top loss coefficient f: a: absorption coefficient f: transmission coefficient f: collactor top loss coefficient f: collactor coefficient f: transmission coefficient f: collactor co	U_b : collector back loss coefficient (W/m ²⁰ C)	19212 C V
$\begin{aligned} u_{i} & \text{is transmission coefficient} \\ & \text{T}_{i} : \text{Bricheavery} (\mathbb{C}) \\ & \text{T}_{i} : \text{abselut temperature} (\mathbb{C}) \\ & \text{C} : \text{Specific heat of air (Dkg oC)} \\ & \text{miss flow rate (kg/s)} \\ & \text{H} : \text{collector height(m)} \\ & \text{k: thermal conductivity (W/m "C)} \\ & \text{A : area (m^2)} \\ \\ & \begin{array}{c} & & \\ &$	U ₁ : collector top loss coefficient (W/m ⁻⁺ C)	$\left(\frac{2h_{e}l}{2}\right)^{a}$
$ \begin{aligned} & \varepsilon : \text{amissivity} \\ & \eta : \text{Efficiency} \\ & g : \text{solar realistion}(W/m^2) \\ & T_{j} : \text{PV} \text{ temperature (°C)} \\ & T_{i} : \text{ abseluate temperature (°C)} \\ & H_{i} : \text{ collector height(m)} \\ & H_{i} : \text{ area (m^2)} \end{aligned} \qquad $	τ : transmission coefficient	$M = \left(\frac{k}{k}\right)$
$\begin{split} & \eta: \text{Efficiency} \\ & g: \text{solar radiation}(W/m^2) \\ & f_p: \text{PV temperature}(^{\circ}\text{C}) \\ & f_p: \text{PV temperature}(^{\circ}\text{C}) \\ & f_p: \text{PV temperature}(^{\circ}\text{C}) \\ & f_r: \text{abjent temperature}(^{\circ$	s : emissivity	('n 'en)
$\begin{aligned} & D_{1} = 0^{1} \operatorname{conderted matrix}(V(M)) & T_{1} & T_{1} \\ & T_{2} = 1^{1} \operatorname{conderted matrix}(C) \\ & T_{1} : D_{2} \operatorname{conderted matrix}(T) \\ & T_{1} : D_{2} = T_{1} : \\ & T_{1} : D_{2} : D_{$	η : Efficiency	$U_{k} = \frac{\kappa_{l}}{2}$
$\begin{split} \begin{array}{l} T_{b}: \operatorname{back} p \operatorname{late temperature} (^{\circ}\mathrm{C}) \\ T_{a}: \operatorname{ambient temperature} (^{\circ}\mathrm{C}) \\ T_{a}: \operatorname{ambient temperature} (^{\circ}\mathrm{C}) \\ C: \operatorname{Specific heat of air} (Jkg \circ C) \\ m: \operatorname{mass} flow rate (kg's) \\ H: \operatorname{collector height} (m) \\ k: \operatorname{thermal conductivity} (W/m ^{\circ}\mathrm{C}) \\ A: \operatorname{area} (m^{2}) \end{split} \qquad $	T.: PV temperature (°C)	$^{\nu}$ I_{t}
$T_{i:\text{ ambient temperature (°C)}} T_{i:\text{ subject temperature (°C)}} U_{i} = \left \frac{1}{h_{w} + h_{pu}} \right $ $C: \text{Specific heat of air (Jkg oC)}$ $m: \max s flow rate (kg's)$ $H: collector height (m)$ $k: \text{ thermal conductivity (W/m °C)}$ $A: \operatorname{area}(m^{2})$ $h_{pu} = \frac{\sigma(T_{p} + T_{b})(T_{p}^{2} + T_{b}^{2})}{\left(\frac{1}{\varepsilon_{p}} + \frac{1}{\varepsilon_{b}} - 1\right)}$ $h_{pu} = \varepsilon_{p}\sigma(T_{p}^{2} + T_{dy}^{2})(T_{p} - T_{dy})$ $T_{aly} = 0.0522 T_{a}^{1.5}$ $h_{1} = h_{c}$	Th: back plate temperature (°C)	(· ·) ⁻¹
$h_{r,s} = \frac{c_{r}}{c_{r}} \left(h_{w} + h_{ryw} \right)$ $h_{ryw} = \frac{c_{r}}{c_{r}} \left(\frac{1}{c_{p}} + \frac{1}{c_{s}} \right)$ $h_{ryw} = c_{p} \left(\frac{1}{c_{p}} + \frac{1}{c_{s}} \right)$ $h_{ryw} = 0.0522 T_{a}^{1.5}$ $h_{r} = h_{c}$	T _s : ambient temperature (°C)	$U_{i} = \frac{1}{1}$
$h_{rpb} = \frac{\sigma(T_p + T_b)(T_p^2 + T_b^2)}{\left(\frac{1}{\varepsilon_p} + \frac{1}{\varepsilon_p} - 1\right)}$ $h_{rpb} = \frac{\sigma(T_p + T_b)(T_p^2 + T_b^2)}{\left(\frac{1}{\varepsilon_p} + \frac{1}{\varepsilon_p} - 1\right)}$ $h_{rpa} = \varepsilon_p \sigma(T_p^2 + T_{sby}^2)(T_p - T_{sby})$ $T_{sby} = 0.0522 T_a^{1.5}$ $h_1 = h_c$	Γ _s :sky temperature (°C) C : Snecific heat of air (1/k π oC)	$(h_w + h_{rpa})$
H: collector height (m) k: thermal conductivity (W/m °C) A: area (m ²) $h_{rpb} = \frac{O(x_p + 1_b)A_p + 1_b}{\left(\frac{1}{\varepsilon_p} + \frac{1}{\varepsilon_b} - 1\right)}$ $h_{rpa} = \varepsilon_p \sigma \left(T_p^2 + T_{ky}^2\right) \left(T_p - T_{sky}\right)$ $T_{sky} = 0.0522 T_a^{1.3}$ $h_1 = h_c$	m : mass flow rate (kg/s)	$\sigma(T + T)(T^2 + T^2)$
k : thermal conductivity (W/m ⁻ C) A : area (m ²) $\begin{pmatrix} \frac{1}{\varepsilon_p} + \frac{1}{\varepsilon_b} - 1 \\ h_{rpa} = \varepsilon_p \sigma (T_p^2 + T_{ky}^2) (T_p - T_{sky}) \\ T_{sky} = 0.0522 T_a^{1.5} \\ h_1 = h_c = h_c$	H : collector height (m)	$h_{rpb} = \frac{O(I_p + I_b)(I_p + I_b)}{O(I_p + I_b)}$
$h_{pa} = \varepsilon_p \sigma \left(T_p^2 + T_{dy}^2\right) \left(T_p - T_{dy}\right)$ $h_{qu} = h_p \sigma \left(T_p^2 + T_{dy}^2\right) \left(T_p - T_{dy}\right)$ $T_{dy} = 0.0522 T_a^{1.5}$ $h_1 = h_2 = h_c$	k : thermal conductivity (W/m °C)	$\left(\frac{1}{1} + \frac{1}{1} - 1\right)$
$h_{rpa} = \varepsilon_p \sigma \left(T_p^2 + T_{sky}^2\right) \left(T_p - T_{sky}\right)$ $T_{sky} = 0.0522 T_a^{1.3}$ $h_1 = h_2 = h_c$	A. area (m.)	$\left(\overline{\varepsilon_p}^+, \overline{\varepsilon_b}^-\right)$
$T_{aby} = 0.0522 T_a^{1.5}$ $h_1 = h_2 = h_c$		$h_{rps} = \varepsilon_p \sigma \left(T_p^2 + T_{sky}^2\right) \left(T_p - T_{sky}\right)$
$h_1 = h_2 = h_c$		$T_{sky} = 0.0522 T_a^{1.5}$
		$h_1 = h_2 = h_c$

Tables 2. The studies conducted of PVT systems

Year	Author(s)	PVT systems	Ene	Energy efficiency (%)		PVT
			PVT	PV	Thermal	Exergy efficiency
2018	Fudholi et al. [21]	PVT air collector with ∇ -groove	31.21-	9.87-	21.3-82.9	12.66-12.91
2017	Salem [22]	Hybrid PVT system	59.3-92	17.7-	31.6-57.9	11.1-13.5
2017	Lari & Sahin [23]	PVT nanofluid system	NA	13.2	NA	NA
2016	Khanjari [24]	PVT nanofluid system	90	10-13.7	55	15
2016	Tripathi et al. [25]	PVT concentrating collector	45-63	NA	40-50	NA
2016	Singet al. [26]	Active solar still integrated with two hybrid PVT collectors	69.06	NA	75	NA
2016	Hazami et al. [27]	PVT air collector system	NA	15	50	14.8
2016	Gholampour & Ameri	PVT flat transpired air collectors	55	NA	69.91	8.66
2016	Tiwari & Tiwari [29]	PVT mixed mode greenhouse solar dryer	68.5	NA	NA	NA
2015	Rajoria et al. [30]	Semitransparent PVT air collector	NA	3.1-9.1	12.1-28.1	NA
2015	Jahromi et al. [31]	Commercially available PVT water collector	NA	7.5-8.7	51.6-52	9.6-9.7
2015	Tiwari et al. [32]	PV flat plate collector active solar	28.5-	NA	13.4-23.2	NA
2014	Ibrahim et al.[33]	PVT water collector	55-62	11.4	45-51	12.0-14.0
2014	Kamthania & Tiwari	Semi-transparent hybrid PVT double	NA	12	NA	NA
2013	Rajoria et al. [35]	Novel hybrid PVT air collector	11.3	NA	NA	16.3
2013	Mishra & Tiwari [36]	Hybrid PVT water collector	NA	10.0-	28.2-45.9	NA
2012	Agrawal et al. [37]	Glazed hybrid PVT tiles air collector	NA	12.4	35.7	NA
2011	Gang et al. [38]	Heat pipe PVT system	NA	9.4	41.9	6.8
2011	Agrawal & Tiwari [39]	Hybrid micro-channel PVT air collector	NA	NA	NA	9.38-18.03
2011	Wu et al. [40]	Heat pipe PVT hybrid system	NA	8.45	63.65	10.26
2010	Sarhaddi et al. [41]	PVT air collector	45	10	17.18	10.75
2010	Agrawal & Tiwari [42]	BIPVT systems	NA	7.13	33.54	NA
2010	Agrawal & Tiwari [43]	BIPVT systems	53.7	NA	NA	NA

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4. CONCLUSION

Based on the present review, the following conclusions can be drawn; 1) A number of research have been done on PVT systems over the last four decades, exploring aspects such as efficiency enhancements by design development, numerical simulation, prototype design, experimental testing and testing methodologies for PVT systems, 2) The development of PVT system is a very promising area of research. Today, PVT systems using in various applications, such as solar drying, solar cooling, water heating, desalination, and pool heating.

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Ahmad Fudholi, Ph.D, M.Sc obtained his S.Si (2002) in physics. He was born in 1980 in Indonesia, and has working experience about 4 years (2004-2008) as Head of Physics Department at Rab University Pekanbaru, Riau, Indonesia. A. Fudholi started his master course in Energy Technology (2005-2007) at Universiti Kebangsaan Malaysia (UKM). After his master he became Research Assistant at UKM up to 2012. After his Ph.D (2012) in renewable energy, he became Postdoctoral in Solar Energy Research Institute (SERI) UKM up to 2013. He joined the SERI as a Lecture in 2014. More than USD 310,000 research grant (13 grant/ project) in 2014-2017 was involved. More than 25 M.Sc project supervised and completed. Until now, he managed to supervise 5 Ph.D (4 main supervisor and 1 Co. supervisor), 3 Master's student by research mode, and 5 Master's student by coursework mode, he was also as examiner (3 Ph.D and 1 M.Sc). His current research focuses on renewable energy, especially solar energy technology, micropower system, solar drying systems, and advanced solar thermal systems (solar assisted drying, solar heat pump, PVT systems). He has published more than 100 peer-reviewed papers, which 25 papers in ISI index (20 Q1, impact factor more than 3) and more than 50 papers in Scopus index, 16 more currently accepted manuscript, 20 more currently under review, and 2 book chapters. Addition, he has published more than 70 papers in international conferences. His total citations of 609 by 419 documents and h-index of 12 in Scopus (Author ID: 57195432490). His total citations of 1132 and h-index of 19 in google scholar. He is appointed as reviewer of high impact (Q1) journal such as Renewable and Sustainable Energy Reviews, Energy

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Prof Dato' Dr. Kamaruzzaman Sopian graduated with the BS Mechanical Engineering from the University of Wisconsin-Madison in 1985, the MS in Energy Resources University of Pittsburgh in 1989 and PhD in Mechanical Engineering from the Dorgan Solar Laboratory, University of Miami at Coral Gables in 1997. He was promoted to the post of Professor of Renewable Energy in the Department of Mechanical and Material Engineering, at the UKM Malaysia in 2001 and currently is the Director of the Solar Energy Research Institute in the same university since 2005. He has been involved in the field of renewable energy for more than 25years. His main contributions are in solar radiation modeling and resource assessment, advanced solar photovoltaic systems and advanced solar thermal systems. He has secure research funding from the Malaysian Minstry of Science and Malaysian Ministry of Education and industry for more than USD 6 million. He has conducted renewable enery courses the Asian School of Energy (2007-2014) funded by ISESCO, COMSAT, TIKA and UNESCO. He has published over 800 research papers in journals and conferences (SCOPUS h index = 49, no. of citation = 8001) (Google Scholar h index = 60, no. of citation = 13473). A total of 32 MSc (coursework), 15 MSc (research mode) and 50 PhD candidates from various countries. He has undertaken short assignments in about 10 countries for international agencies and programs such as UNDP-GEF, UNIDO, ASEAN EU-Energy Facility, ASEAN-Australia Economic Co-operation Program, ASEAN-CIDA, JSPS-VCC, British Council CHICHE, ISESCO and UNESCO related to renewable energy technology. He has been appointed as the Honorary Professor of Renewable Energy, at University of Nottingham, United Kingdom (2009-2013). In addition, he has been appointed as the associate editors in high impact journals. He won several international awards for his academic contribution in renewable energy including the IDB (Islamic Development Bank) S&T Prize 2013, World Renewable Energy Network Pioneer Award 2012, Malaysia Green Technology Award 2012, and the ASEAN Energy Awards (2005, 2007, 2013 and 2014). He has 4 patents, 20 patents pending, 6 copyrights, and 1 trademark for his innovation in renewable energy technology. The innovation and invention in renewable energy technology have won 80 medals in national and international innovation and invention competitions including special innovation awards such as Prix de L 'Environnement by the Swiss Society for Environmental Protection, 2001, Geneva, Sustainable Development Award INNOVA 2007, Special Prize, Korea Invention Promotion Association at the INPEX Pittsburgh 2008 and Energy and Environmental Award, at INNOVA 2013 in Brussels. His Royal Highness The Sultan of Perak conferred the Paduka Mahkota Perak and the Dato' Paduka Mahkota Perak in 2013. He was conferred as a Fellow of the Malaysia Academy of Sciences (FASc) in 2011.